

## Supporting Information

### **Catalytic Thiophene Oxidation by Groups 4 and 5 Framework-Substituted Zeolites with Hydrogen Peroxide: Mechanistic and Spectroscopic Evidence for the Effects of Metal Lewis Acidity and Solvent Lewis Basicity**

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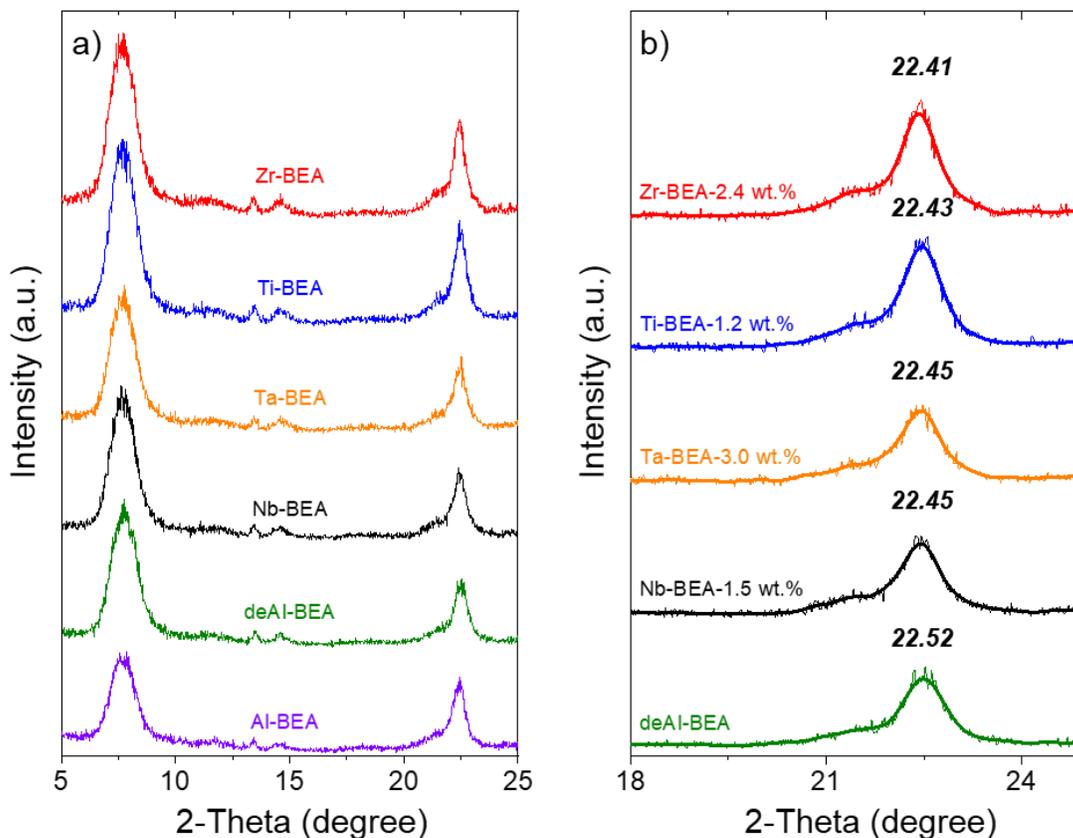
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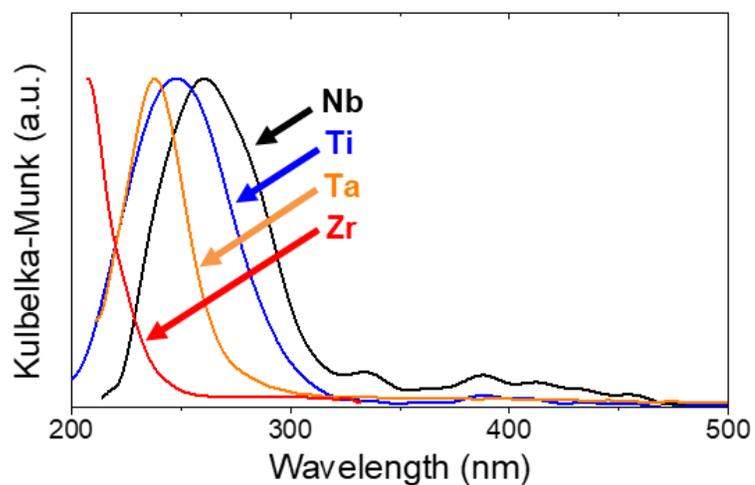
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## S1.0 Additional Catalyst Characterization and the Absence of Mass-Transfer Restrictions

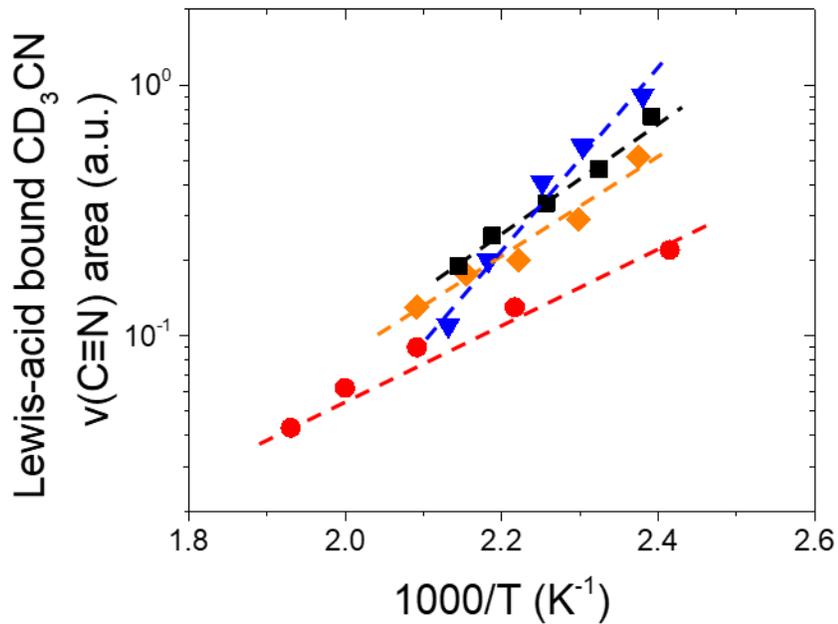
### S1.1 Catalyst Characterization



**Figure S1.** X-ray diffractograms for (a) Zr-BEA, Ti-BEA, Ta-BEA, Nb-BEA, dealuminated \*BEA, and Al-BEA (i.e., the parent \*BEA) used in the kinetic studies (Section 3 of the main text) and (b) of Zr-BEA, Ti-BEA, Nb-BEA, Ta-BEA, with weight loadings of 2.4, 1.2, 3.0, and 1.5 wt.%, respectively, and dealuminated BEA\* to visualize changes in the peak position of the ~22.5 degree X-ray diffractogram feature. Bold solid lines in (b) represent a finite Fourier transform to smooth the data with 10 points of fitting.

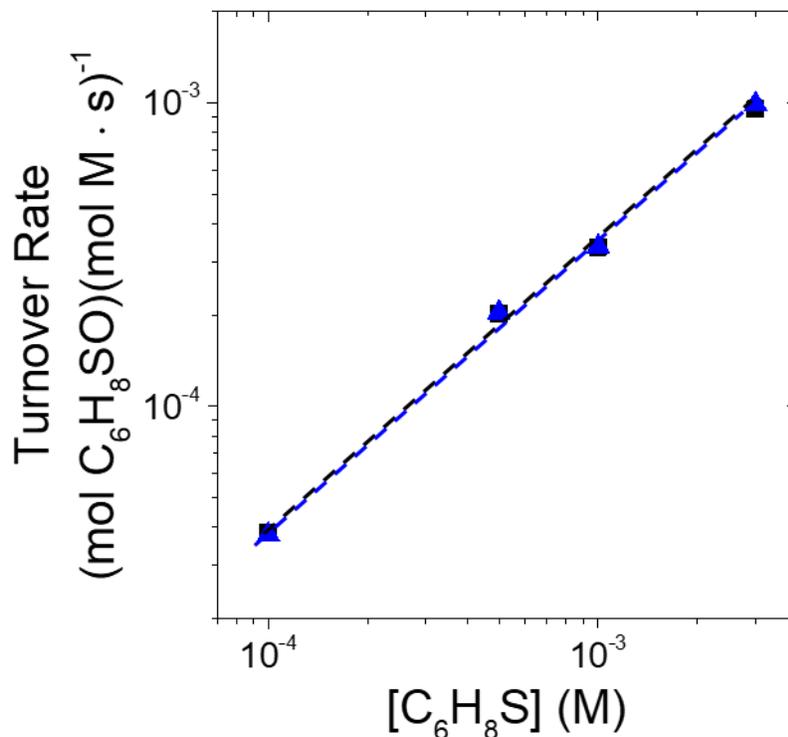


**Figure S2.** Normalized diffuse reflectance UV-vis spectra of Ti- (blue), Nb- (black), Ta- (orange), and Zr- (red) BEA materials diluted in a 1:10 by weight ratio with MgO. Pure MgO was used as the background. Spectral artifacts at >325 nm for Ti- and Nb-BEA arise from smoothing with a finite fourier transform with 10 points of smoothing.



**Figure S3.** IR feature areas for Lewis-acid bound CD<sub>3</sub>CN on Ti-BEA (blue ▼, 2302 cm<sup>-1</sup>), Nb-BEA (black ■, 2306 cm<sup>-1</sup>), Ta-BEA (orange ◆, 2312 cm<sup>-1</sup>), and Zr-BEA (red ●, 2296 cm<sup>-1</sup>) as a function of inverse temperature (1.5 kPa CD<sub>3</sub>CN, 100 kPa He, 50 cm<sup>3</sup> min<sup>-1</sup>) after background subtraction. Dashed lines represent linear fits, whose slopes are proportional to the value of  $\Delta H_{\text{CD}_3\text{CN}}$ .

## S1.2 Experimental Verification for the Absence of Mass-Transfer Restrictions

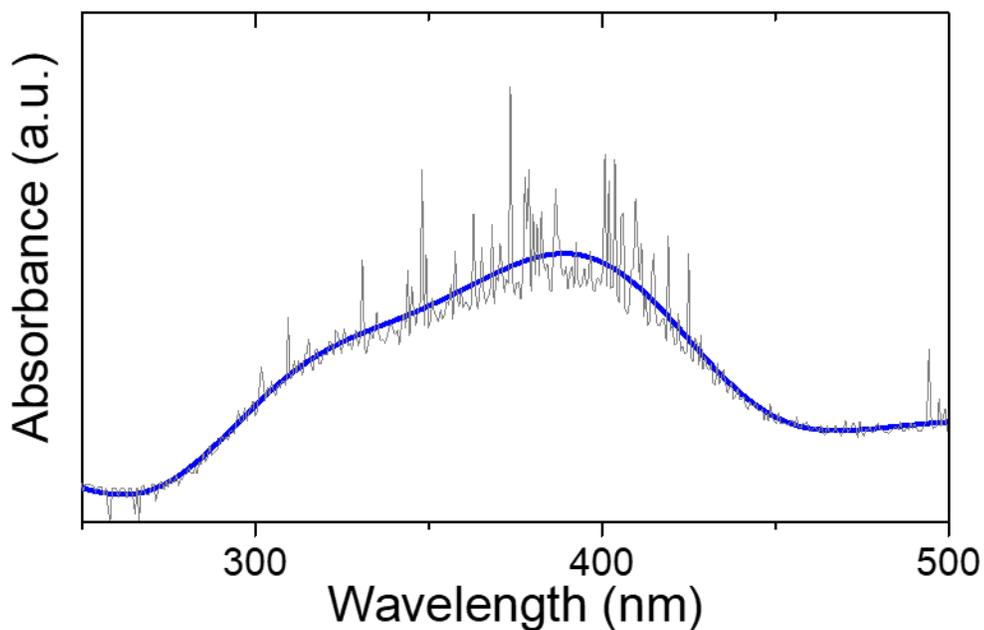


**Figure S4.** Turnover rates for the formation of  $C_6H_8SO$  measured as a function of  $[C_6H_8S]$  on Ti-BEA (blue solid ▲, 0.141 wt.% Ti, used in kinetics experiments in main text; 0.01 M  $H_2O_2$ , 313 K) and Ti-BEA (black ■, 0.019 wt.% Ti; 0.01 M  $H_2O_2$ , 313 K). Dashed lines are intended to guide the eye.

Figure S5 shows rates for the formation of 2,5-dimethylthiophene oxide ( $C_6H_8SO$ ) measured as a function of  $C_6H_8S$  concentration for multiple metal loadings of Ti (0.141 wt.% and 0.019 wt.%) in Ti-BEA. The rate of  $C_6H_8O$  formation is invariant with metal loading, which indicates that the Madon-Boudart criterion is satisfied for Ti-BEA.[1]

In Fig. 3 (main text),  $C_6H_8SO$  formation rates are highest for Ti-BEA (of all M-BEA and M-SiO<sub>2</sub>) under these conditions, which suggests that satisfaction of the Madon-Boudart criterion for Ti-BEA implies that the other M-BEA (i.e., those with lower turnover rates and similar crystallite size) do not possess mass-transfer restrictions.

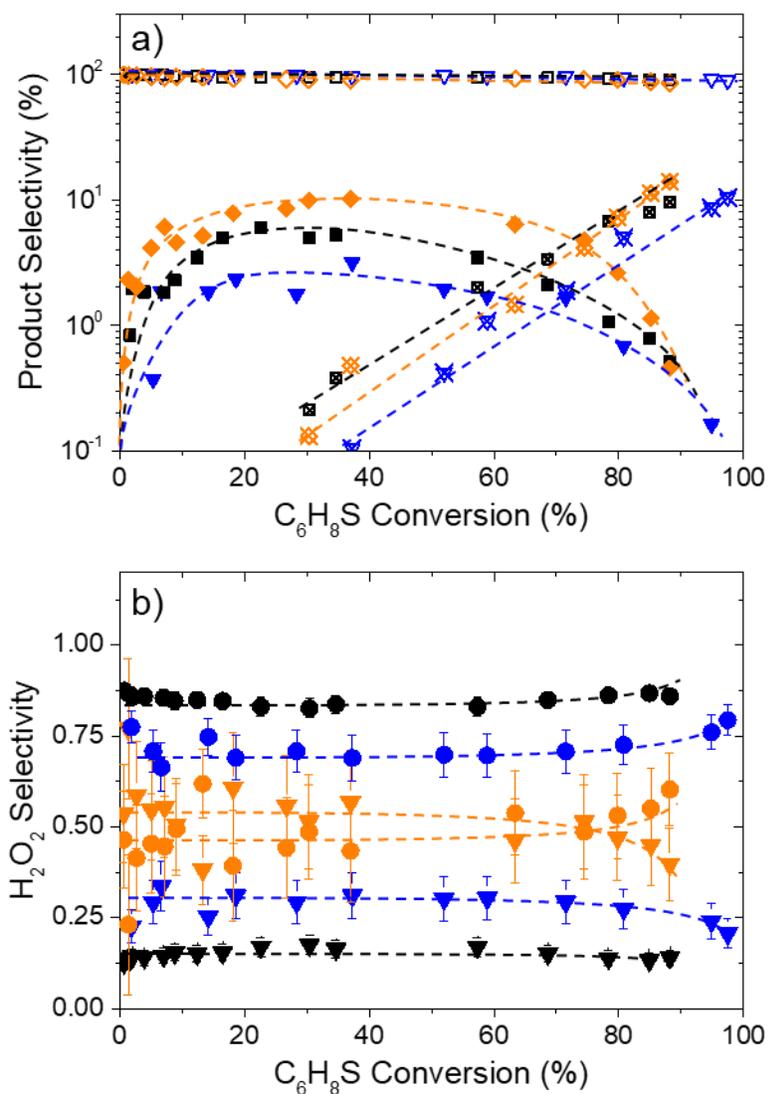
## S2. Sample Raw UV-Vis Spectrum and Spectral Processing



**Figure S5.** UV-vis absorbance spectrum (raw data, gray) of H<sub>2</sub>O<sub>2</sub>-treated Ti-BEA at 313 K in flowing CH<sub>3</sub>CN (0.4 M H<sub>2</sub>O, 0.01 M H<sub>2</sub>O<sub>2</sub>, 313 K) and smoothed data (bold blue line) using a finite fourier transform with 40 points of fitting performed in OriginPro®.

For all UV-vis experiments, spectra were collected at steady state (i.e., where the UV-vis features were unchanging with time) and smoothed using OriginPro® in a systematic fashion (i.e., using the same wavelength intervals and number of smoothing points).

#### S4. Product Selectivities over M-BEA



**Figure S6.** (a) Product selectivity towards C<sub>6</sub>H<sub>8</sub>SO (open symbols), C<sub>6</sub>H<sub>8</sub>SO<sub>2</sub> (closed symbols), and C<sub>6</sub>H<sub>8</sub>SO<sub>3</sub> (symbols with a “X”) over Ti-BEA (blue ▼), Nb-BEA (black ■), and Ta-BEA (orange ◆) and (b) H<sub>2</sub>O<sub>2</sub> selectivity towards oxidation (▼) and H<sub>2</sub>O<sub>2</sub> decomposition (●) as a function of C<sub>6</sub>H<sub>8</sub>S conversion (5 mM C<sub>6</sub>H<sub>8</sub>S, 0.05 H<sub>2</sub>O<sub>2</sub>, 313 K) over Ti-BEA (blue), Nb-BEA (black), and Ta-BEA (orange). Dashed curves are intended to guide the eye.

## S5 Supplemental Information for the Derivation of Rate Expression for Sulfoxidation and Transition State Theory

### S5.1 Pseudo Steady State Hypothesis Applied to M-(O<sub>2</sub>) Intermediates

The pseudo steady state hypothesis (PSSH) assumes that the concentration (or number) of a specific reactive species is unchanging with time during a reaction. Application of the PSSH to M-(O<sub>2</sub>) intermediates in section 3.3, results in the following expression:

$$\frac{d[M-(O_2)]}{dt} \approx 0 = k_3[H_2O_2^*] - k_4[C_6H_8S][M-(O_2)] + k_5[H_2O_2][M-(O_2)] + k_7[C_6H_8SO][M-(O_2)] \quad (S1)$$

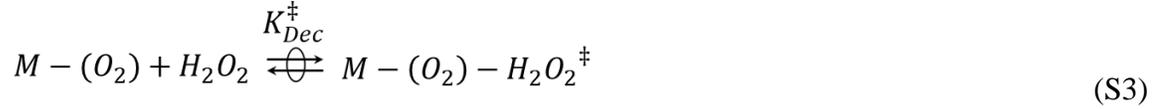
where  $k_x$  represents the rate constant for step  $x$ ,  $[M-(O_2)]$  is the number of M-(O<sub>2</sub>) intermediates,  $[H_2O_2^*]$  is the number of H<sub>2</sub>O<sub>2</sub> molecules bound to active sites, and all other species within brackets ([ ]) are the corresponding liquid-phase concentrations. When H<sub>2</sub>O<sub>2</sub> adsorption is assumed to be quasi-equilibrated (step 2, Scheme 1), equation S1 can be rearranged to yield:

$$[M-(O_2)] = \frac{k_3 K_2 [H_2O_2] [*]}{k_4 [C_6H_8S] + k_5 [H_2O_2] + k_7 [C_6H_8SO]} \quad (S2)$$

where [\*] is the number of unoccupied (or solvent-covered) active sites. Equation S2 is then combined with equation 1 (main text) to yield equation 2 from the main text.

## S5.2 Transition State Theory for Measurement of Activation Enthalpies and Entropies

Application of TST assumes that the state immediately preceding the transition state and the transition state are in equilibrium [2], which takes the form of



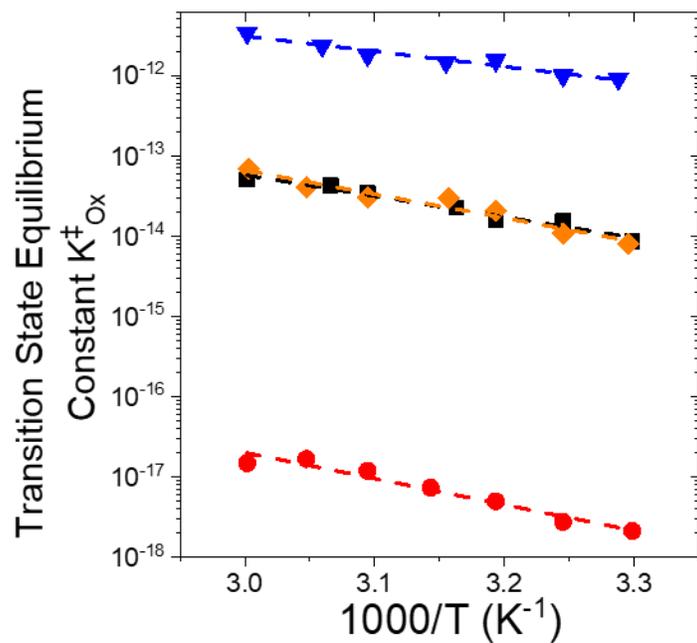
where  $M-(O_2)-H_2O_2^\ddagger$  and  $K_{Dec}^\ddagger$  represent the transition states and transition state equilibrium constants for  $H_2O_2$  decomposition, respectively. The rates for  $H_2O_2$  decomposition can then be expressed in terms of the numbers of transition states, resulting in

$$\frac{r_{Dec}}{[L]} = \frac{k_b T}{h} [M - (O_2) - H_2O_2^\ddagger] \quad (S4)$$

where  $T$  is the absolute temperature in Kelvin and  $k_b$  and  $h$  are Boltzmann's and Planck's constants, respectively. Measurement of the reaction rates under a  $M-(O_2)$  MASI allows equation 2 to be re-expressed as

$$\frac{r_{Dec}}{[L]} = \frac{k_b T}{h} K_{Dec}^\ddagger [H_2O_2] \quad (S5)$$

which allows for  $K_{Dec}^\ddagger$  to be determined by measurement of turnover rates for each reaction pathway at a given temperature.



**Figure S7.** Transition state equilibrium constants for C<sub>6</sub>H<sub>8</sub>S oxidation ( $K^{\ddagger}_{Ox}$ ) as a function of inverse temperature on Ti-BEA (blue ▼, 3 mM C<sub>8</sub>H<sub>8</sub>, 0.01 M H<sub>2</sub>O<sub>2</sub>), Nb-BEA (black ■, 3 mM C<sub>8</sub>H<sub>8</sub>, 1 mM H<sub>2</sub>O<sub>2</sub>), Ta-BEA (orange ◆, 3 mM, 1 mM H<sub>2</sub>O<sub>2</sub>), and Zr-BEA (red ●) in CH<sub>3</sub>CN. Dashed lines represent fits to the Eyring equation whose slopes are proportional to  $\Delta H^{\ddagger}$ .

**References:**

- [1] R.J. Madon, M. Boudart, Experimental Criterion for the Absence of Artifacts in the Measurement of Rates of Heterogeneous Catalytic Reactions, *Ind. Eng. Chem. Fundam.*, 21 (1982) 438-447.
  
- [2] I. Chorkendorff, J.W.H. Niemantsverdriet, *Concepts of Modern Catalysis and Kinetics*, 2<sup>nd</sup> ed., Wiley-VCH Verlag GmbH & Co., Weinheim, 2007.